

IN THE CLAIMS

Please amend the claims as follows:

Claim 1 (Currently Amended): A process for preparing 1,6-hexanediol from a carboxylic acid mixture ~~which comprises~~ comprising adipic acid, 6-hydroxycaproic acid and small amounts of 1,4-cyclohexanediols and is obtained as a by-product in the oxidation of cyclohexane to cyclohexanone/cyclohexanol with oxygen or oxygen-containing gases and by water extraction of the reaction mixture, by esterification of the acids with C₁- to C₁₀-alcohols and hydrogenation, in which

a) the mono- and dicarboxylic acids present in the aqueous dicarboxylic acid mixture are reacted with a low molecular weight alcohol to give the corresponding carboxylic esters,

b) the resulting esterification mixture is freed of excess alcohol and low boilers in a first distillation stage,

c) a separation of the bottom product is carried out in a second distillation stage ~~into to form~~ into to form an ester fraction substantially free of 1,4-cyclohexanediols and a fraction comprising at least the majority of the 1,4-cyclohexanediols,

d) the ester fraction substantially free of 1,4-cyclohexanediols is catalytically hydrogenated and

e) 1,6-hexanediol is obtained in a purifying distillation stage from the hydrogenation effluent while removing an alcohol-low boiler mixture ~~in a manner known per se~~,

which comprises removing alcohol by a membrane system from the mixtures, obtained after the esterification in stage b) and/or after the hydrogenation in stage e), of alcohols and low boilers and recycling it into the esterification.

Claim 2 (Original): The process according to claim 1, wherein alcohol is removed by a membrane system from the mixtures obtained in stage b) and stage e).

Claim 3 (Currently Amended): The process according to claim 1 ~~or 2~~, wherein methanol is removed.

Claim 4 (Currently Amended): The process according to ~~any of claims 1 to 3~~ claim 1, wherein the membrane system consists of at least one membrane.

Claim 5 (Currently Amended): The process according to ~~any of claims 1 to 4~~ claim 1, wherein the transmembrane pressure differential is from 20 to 200 bar.

Claim 6 (Currently Amended): The process according to ~~any of claims 1 to 4~~ claim 1, wherein the temperature of the mixture obtained in stage b) and/or e), as the feed stream of the membrane separation, is from 20 to 90°C.